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# Robust control and observation of nonlinear processes using discontinuities

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# Overview

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- 1 Introduction
- 2 Exact State and Input Observers for Nonlinear Systems
  - Problem formulation
  - Observer with discontinuous injection
  - Unknown input estimation in a bioreactor
    - Simulation results
- 3 Multivalued Observers
  - The unobservable system considered
  - Observability analysis
  - A bivalued observer for the bioreactor
- 4 Discontinuous Integral Controller
  - SISO Regulation and Tracking Problem
  - The Discontinuous Integral Controller
  - Example: Magnetic Suspension System
- 5 Conclusions

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- Discontinuities are useful for dealing with uncertainties and perturbations in control and observation: Sliding Mode control, switching control, hybrid control, ...
- A possible explanation: Discontinuities are simple models of a large class of signals and help in the estimation and compensation of uncertainties and perturbations.
- Objective:
  - Illustrate this in three control/estimation problems.
  - Some lessons learned from simple bioprocesses and how discontinuities can help in their solution.

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- Estimation of states and (unknown) inputs (e.g. reaction rates, faults, ...) is an important topic.
- **Challenge:** input signals do not have a finite dimensional model  $\Rightarrow$  continuous observers can only **approximately** estimate them, using:
  - High Gains, or
  - Finite dimensional signal models  $\Rightarrow$  increases the observer dimension.
- But an Observer with **discontinuous** output injection term solves exactly the problem for the class of Lipschitz continuous inputs!  $\Rightarrow$  Simple Observer.

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# Problem formulation

Nonlinear (second order) system [Moreno and Dochain, 2013]

$$\dot{z}_1 = g_1(z_1, z_2, u)$$

$$\dot{z}_2 = g_2(z_1, z_2, u)$$

$$y = h(z_1, z_2)$$

- state:  $z = [z_1, z_2] \in \mathcal{Z} \subseteq \mathbb{R}^2$
- unknown input:  $u \in U \subset \mathbb{R}$ .
- $\mathcal{Z}, U$  compact and connected.
- $g_i(z_1, z_2, u)$  ( $i = 1, 2$ ),  $h(z_1, z_2)$  smooth functions.
- Measured variable:  $y$
- Problem: Using  $y$  estimate robustly and in finite time both  $z$  and  $u$ .

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# Model extension and Observability

- **Assumption:**  $u(t)$  Lipschitz continuous, i.e.  $|\dot{u}(t)| \leq \alpha$ .
- **State Extension:**  $z_3 = u$ ,  $\dot{z}_3 = \dot{u} = g_3(t)$ , where  $g_3(t)$  is *unknown*, integrable and bounded, i.e.  $|g_3(t)| \leq \alpha$ ,
- **Assumption:** Strong Observability. i.e. The observability map

$$\mathcal{O}(z) = \begin{bmatrix} h(z) \\ L_g h(z) \\ L_g^2 h(z) \end{bmatrix} = \begin{bmatrix} y \\ \dot{y} \\ \ddot{y} \end{bmatrix}$$

$\Leftrightarrow$  Observability of  $(z_1, z_2)$  for any unknown  $u$  +  
"observability" of  $u$ .

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# Observability form

With transformation  $x = \mathcal{O}(z)$

$$\dot{x}_1 = x_2$$

$$\dot{x}_2 = x_3$$

$$\dot{x}_3 = K(x) + U(x, \dot{u})$$

$$y = x_1,$$

- $K(x)$  *known* term,
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- Assumptions  $\Rightarrow |U(x, \dot{u})| \leq \mu$ .
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# Solvability of the problem: Discussion

- For a **continuous** observer is impossible to estimate  $z$  and  $u$ .
- Reason: The class of signals  $|\dot{u}(t)| \leq \alpha$  is too large!  
(infinite dimensional).
- You need a finite dimensional model of  $u$  for convergence  
→ complex observer!
- But a **discontinuous** observer can → Magic of discontinuity!  
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# Observer with discontinuous injection

$$\dot{\hat{x}}_1 = -Lk_1 [\hat{x}_1 - x_1]^{\frac{2}{3}} + \hat{x}_2$$

$$\dot{\hat{x}}_2 = -L^2k_2 [\hat{x}_1 - x_1]^{\frac{1}{3}} + \hat{x}_3$$

$$\dot{\hat{x}}_3 = -L^3k_3 [\hat{x}_1 - x_1]^0 + K(\hat{x})$$

$$\hat{y} = \hat{x}_1$$

- $|z|^p = |z|^p \text{sign}(z)$
- Estimates  $x$  in finite time for all  $|\dot{u}(t)| \leq \alpha$ .
- Gains  $k_1 > 0$ ,  $k_2 > 0$  and  $k_3 > 0$ ,  $L > 0$  appropriately selected.
- Critical term: sign function  $[\hat{x}_1 - x_1]^0$ .
- Structure borrowed from Levant's differentiator (A. Levant, 2003).
- Structure similar to a High Gain Observer (HGO).

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## Observer in original coordinates

$$\begin{bmatrix} \dot{\hat{z}}_1 \\ \dot{\hat{z}}_2 \\ \dot{\hat{u}} \end{bmatrix} = \begin{bmatrix} g_1(\hat{z}_1, \hat{z}_2, \hat{u}) \\ g_2(\hat{z}_1, \hat{z}_2, \hat{u}) \\ 0 \end{bmatrix} + \\ - J_{\mathcal{O}}^{-1}(\hat{z}_1, \hat{z}_2, \hat{u}) \begin{bmatrix} Lk_1 |\hat{y} - y|^{\frac{2}{3}} \\ L^2 k_2 |\hat{y} - y|^{\frac{1}{3}} \\ L^3 k_3 |\hat{y} - y|^0 \end{bmatrix} \\ \hat{y} = h(\hat{z}_1, \hat{z}_2)$$

$J_{\mathcal{O}}^{-1}(\hat{z}_1, \hat{z}_2, \hat{u})$  inverse of the Jacobian matrix of observability map  $\mathcal{O}(\hat{z}_1, \hat{z}_2, \hat{u})$ .

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# Unknown input estimation in a bioreactor

$$R : \begin{cases} \dot{X}(t) = \mu(S)X - DX, \\ \dot{S}(t) = -\frac{\mu(S)X}{Y} + D(S_{in}(t) - S), \\ y = X \end{cases}$$

- $X \geq 0$  biomass,  $S \geq 0$  substrate concentrations,
- $\mu : \mathbf{R}_+ \rightarrow \mathbf{R}_+$  specific growth rate, given by a Monod law

$$\mu(S) = \frac{\mu_0 S}{S + K_S} = \mu_0 r(S)$$

- $D \geq 0$  dilution rate,
- $S_{in}(t) \geq 0$  unknown input substrate concentration  
 $|\dot{S}_{in}| \leq M,$
- $Y > 0$  yield coefficient.

$$\begin{bmatrix} \dot{\hat{X}} \\ \dot{\hat{S}} \\ \dot{\hat{S}}_{in} \end{bmatrix} = \begin{bmatrix} \mu(\hat{S})\hat{X} - D\hat{X} \\ -\frac{\mu(\hat{S})\hat{X}}{Y} + D(\hat{S}_{in} - \hat{S}) \\ 0 \end{bmatrix} +$$
$$- J_{\mathcal{O}}^{-1}(\hat{X}, \hat{S}, \hat{S}_{in}) \begin{bmatrix} Lk_1 \left[ \hat{X} - X \right]^{\frac{2}{3}} \\ L^2 k_2 \left[ \hat{X} - X \right]^{\frac{1}{3}} \\ L^3 k_3 \operatorname{sign}(\hat{X} - X) \end{bmatrix}, \quad (1)$$

## Observer II

where

$$J_{\mathcal{O}}^{-1} = \begin{bmatrix} 1 & 0 & 0 \\ -\frac{(\mu(S)-D)}{\mu'(S)X} & \frac{1}{\mu'(S)X} & 0 \\ \frac{\eta_2(\mu(S)-D)-\eta_1}{(\mu'(S)X)^2 D}, & \frac{\eta_2(X,S)}{(\mu'(S)X)^2 D}, & \frac{1}{\mu'(S)XD} \end{bmatrix}$$

$$\eta_1(X, S, S_{in}) = \left( D(S_{in} - S) - 2\frac{\mu(S)X}{Y} \right) \times \\ (\mu'(S))^2 X + (\mu(S) - D)^2 \mu'(S) X$$

$$\eta_2(X, S) = -\frac{1}{Y}\mu(S)\mu''(S)X^2 - DS\mu''(S)X + \\ -\frac{1}{Y}(\mu'(S))^2 X^2 + 2\mu(S)\mu'(S)X - 3D\mu'(S)X.$$

# Outline

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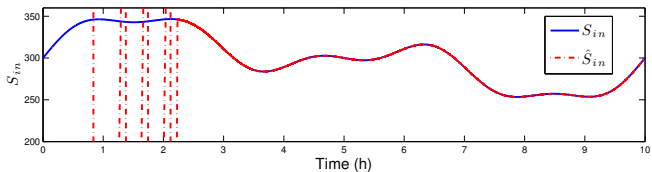
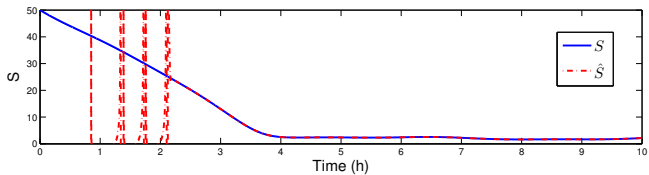
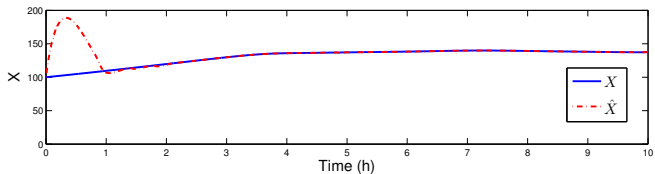
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# Simulation results

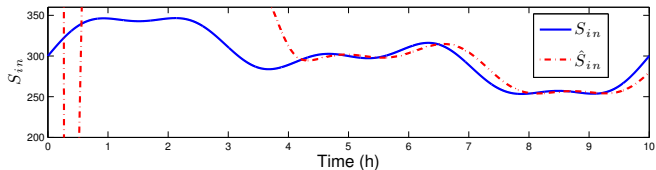
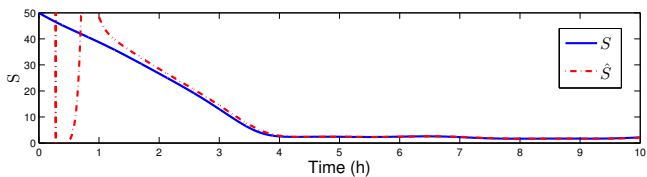
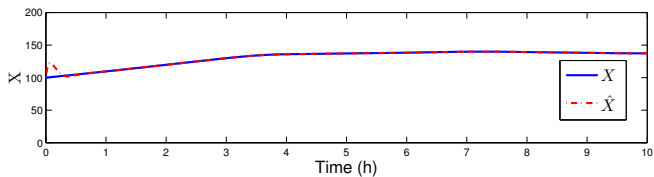
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- Parameters:  $Y = \frac{1}{2}$ ,  $\mu_0 = \frac{1}{5}$ ,  $K_S = 2$ ,  $D = \frac{1}{2}\mu_0$ ,
- Initial Conditions:  $X_0 = 100$ ,  $S_0 = 50$ .
- Observer gains:  $k_1 = 13.2$ ,  $k_2 = 50.82$ ,  $k_3 = 13.31$ ,  $L = 2$ .
- Unknown input  
 $S_{in}(t) = 300 + 30 \sin(0.4\pi t) + 30 \sin(0.2\pi t) + 10 \sin(\pi t)$ .
- $S_{in}(t)$  requires a model of dimension 7.

# Discontinuous observer



# HG observer



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# Introduction

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- Construction of observers is tied to Observability (detectability) properties.
- Local observability is compatible with Global unobservability.
- Observers converge locally but not globally and there is no global observer.
- This phenomenon seems to be common: e.g. chemical reactors, electrical machines (sensorless),...
- A possible solution in case of a finite number of indistinguishable trajectories: reconstruct all possible ones  $\Rightarrow$  Discontinuous injection term.
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# An unobservable bioreactor

$$R: \begin{cases} \dot{X}(t) = \mu(S)X - DX, \\ \dot{S}(t) = -\frac{\mu(S)X}{Y} + D(S_{in}(t) - S), \\ y = X \end{cases}, \quad (2)$$

- $\mu: \mathbf{R}_+ \rightarrow \mathbf{R}_+$  **non-monotonic**, Haldane law

$$\mu(S) = \frac{\mu_0 S}{\frac{S^2}{K_I} + S + K_S} \quad (3)$$

- At  $S^* = \sqrt{K_S K_I}$  achieves its maximum value  $\mu^* = \mu(S^*)$ .
- $D \geq 0$  dilution rate,  $Y > 0$  yield coefficient,
- $S_{in}(t) \geq 0$  unknown input substrate concentration,
- **Problem:** Using  $(X, D)$  estimate  $(S, S_{in})$ .



# Non monotonic reaction rate

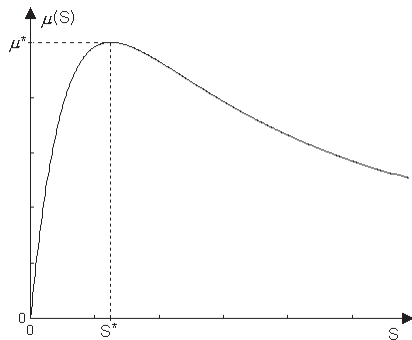


Figure : Haldane Law

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- Monotonic growth rate  $\mu(s)$ 
  - Observability map globally invertible.
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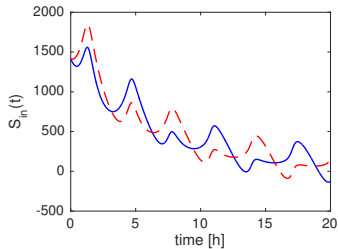
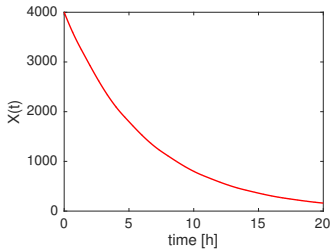
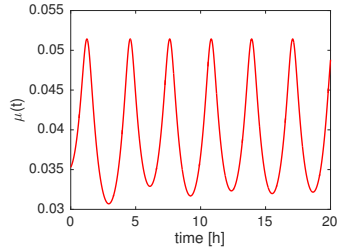
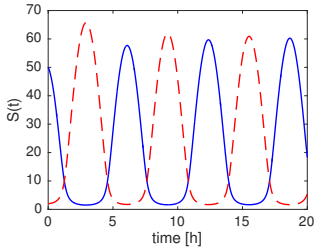
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# Multivalued observers

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For (unobservable) systems with a finite number of indistinguishable trajectories:

- A Global observer does not exist.
- Observers may work locally, but not globally.
- **Multivalued Observer:** Estimate **all** possible indistinguishable trajectories corresponding to the measured variables.
- Possible with **discontinuous** injection terms!



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## A bivalued observer for the bioreactor

$$\dot{\hat{X}}(t) = -k_1 \phi_1(e_X) + \hat{\mu}X - DX, \quad \hat{X}(t_0) = \hat{X}_0,$$

$$\dot{\hat{\mu}}(t) = -k_2 X \phi_2(e_X), \quad \hat{\mu}(t_0) = \hat{\mu}_0,$$

$$\hat{S}_1(t) = \frac{K_I(\mu_0 - \hat{\mu}(t)) - \xi}{2\hat{\mu}(t)}$$

$$\hat{S}_2(t) = \frac{K_I(\mu_0 - \hat{\mu}(t)) + \xi}{2\hat{\mu}(t)},$$

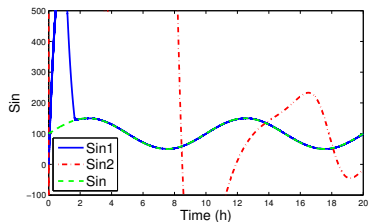
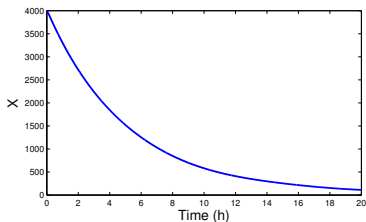
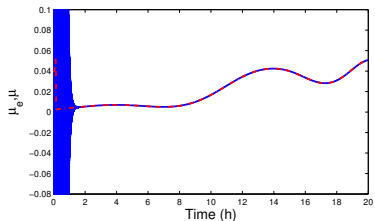
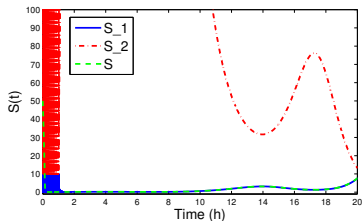
$$\xi = \sqrt{K_I^2(\mu_0 - \hat{\mu}(t))^2 - 4K_S K_I \hat{\mu}^2(t)},$$

$$e_X = \hat{X} - X,$$

$$\phi_1(e_X) = \gamma_1 [e_X]^{\frac{1}{2}} + \gamma_2 e_X, \quad \gamma_1 > 0, \gamma_2 \geq 0,$$

$$\phi_2(e_X) = \frac{\gamma_1^2}{2} [e_X]^0 + \frac{3}{2} \gamma_1 \gamma_2 [e_X]^{\frac{1}{2}} + \gamma_2^2 e_X,$$

# Bivalued Observer Behavior



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# SISO Regulation and Tracking Problem

## SISO smooth, uncertain system

$$\dot{z} = f(t, z) + g(t, z)u, \quad \sigma = h(t, z),$$

- $z \in \mathbb{R}^n$ ,  $u \in \mathbb{R}$ ,  $\sigma \in \mathbb{R}$ : sliding variable/tracking error.
- $f(t, z)$  and  $g(t, z)$  and  $n$  uncertain.
- **Control objective:** to reach and keep  $\sigma \equiv 0$  in finite time.
- Relative Degree  $\rho$  w.r.t.  $\sigma$  is well defined, known and constant.
- Reduced (Zero) Dynamics asymptotically stable (by appropriate selection of  $\sigma$ ).



# The basic DI

Defining  $x = (x_1, \dots, x_\rho)^T = (\sigma, \dot{\sigma}, \dots, \sigma^{(\rho-1)})^T$ ,  $\sigma^{(i)} = \frac{d^i}{dt^i} h(z, t)$

## The regular form

$$\Sigma_T : \begin{cases} \dot{x}_i = x_{i+1}, & i = 1, \dots, \rho - 1, \\ \dot{x}_\rho = w(t, z) + b(t, z)u, & x_0 = x(0), \\ \dot{\zeta} = \phi(\zeta, x) & \zeta_0 = \zeta(0), \end{cases}$$

$$0 < K_m \leq b(t, z) \leq K_M, |w(t, z)| \leq C.$$

## Reduced Dynamics Asymptotically stable:

$$\dot{\zeta} = \phi(\zeta, 0), \quad \zeta_0 = \zeta(0),$$

## The basic Differential Inclusion (DI)

$$\Sigma_{DI} : \begin{cases} \dot{x}_i = x_{i+1}, & i = 1, \dots, \rho - 1, \\ \dot{x}_\rho \in [-C, C] + [K_m, K_M]u. \end{cases}$$

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# Higher Order Sliding Mode (HOSM) Control Solution

## Bounded memoryless feedback controller

$$u = \vartheta_\rho(x_1, x_2, \dots, x_\rho),$$

- A continuous controller  $\vartheta_\rho$  **cannot** solve the problem!
- Reason: The class of perturbations/uncertainties is too large.
- $\vartheta_\rho$  necessarily **discontinuous** at  $x = 0$  for robustness  $[-C, C]$ .
- **Possible explanation:** The discontinuity is a simple model for the class of uncertainties/perturbations.
- Renders  $x_1 = x_2 = \dots = x_\rho = 0$  finite-time stable.
- Motion on the set  $x = 0$  is  $\rho$ th-order sliding mode.
- **Drawback:** Chattering!

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# Discontinuous Integral Controller

## Homogeneous Discontinuous Integral control

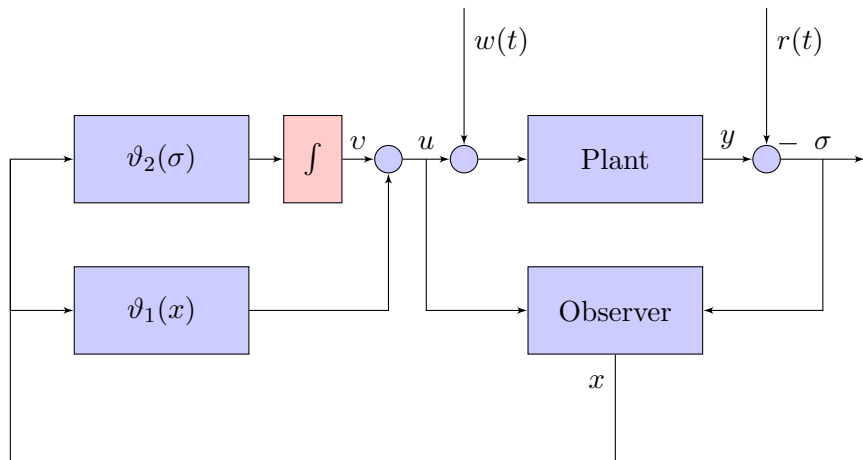
$$\Sigma_T : \begin{cases} \dot{x}_i = x_{i+1}, & i = 1, \dots, \rho - 1, \\ \dot{x}_\rho = u + w(t), & x_0 = x(0), \\ |\dot{w}(t, z)| \leq C. \end{cases}$$

$$\begin{aligned} u &= k_1 \vartheta_1(x_1, x_2, \dots, x_\rho) + x_{\rho+1}, \\ \dot{x}_{\rho+1} &= k_2 \vartheta_2(x_1), \end{aligned}$$

- $\vartheta_1(\cdot)$  homogeneous,
- $\vartheta_2(\cdot)$  homogeneous of degree 0 (discontinuous!),
- Homogeneity:

$$\vartheta_1(\epsilon^{r_1} x_1, \epsilon^{r_2} x_2, \dots, \epsilon x_{r_\rho}) = \epsilon^\delta \vartheta_1(x_1, x_2, \dots, x_\rho) \quad \forall \epsilon > 0$$

# Block Diagram of Discontinuous I-Control



# Virtues of Discontinuous Integral Control

- Continuous control signal  $u(t)$ .
- Continuous ( $\vartheta_2$ ) I-Control rejects/tracks constants  
 $|\dot{w}(t, z)| = 0$ .
- Continuous controllers require a model of the references/perturbations to compensate them  $\Rightarrow$  Internal Model Principle.
- Discontinuous ( $\vartheta_2$ ) I-Control rejects/tracks Lipschitz perturbations/references!  $|\dot{w}(t, z)| \leq C$ .
- Discontinuity is a simple model for the class of perturbations/references.
- Requires only  $x$  and not  $\dot{x}_\rho$ .
- $x_{\rho+1}$  estimates perturbation  $w \Rightarrow$  for  $t \geq T$ ,  
 $x_{\rho+1}(t) = -w(t)$ .
- For  $\rho = 1$ : Super-Twisting!
- Output feedback: using continuous/discontinuous observer!



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# Magnetic Suspension System

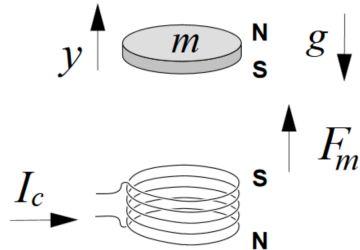


Figure : ECP Model 730: Magnetic Suspension System

# Magnetic Suspension System

$$\dot{x}_1 = x_2$$

$$\dot{x}_2 = -\frac{k}{m}x_2 - \frac{aL_0}{2m} \frac{x_3^2}{(a+x_1)^2} + g$$

$$\dot{x}_3 = \frac{1}{L(x_1)} \left( -Rx_3 + aL_0 \frac{x_2x_3}{(a+x_1)^2} + u \right)$$

$$L(x_1) = L_1 + \frac{aL_0}{a+x_1}$$

- $x_1 = y \in \mathbb{R}_+$ : position of the disc,
- $x_2 = \dot{y} \in \mathbb{R}$ : velocity,
- $x_3 = I_c$ : current in the coil,
- $u = V$ : voltage.

# Discontinuous I-Controller

- Control Objective: Position Tracking error  
 $e_1 = y - r(t) \equiv 0$  after finite time.
- Tracking Error Dynamics

$$\dot{e}_1 = e_2$$

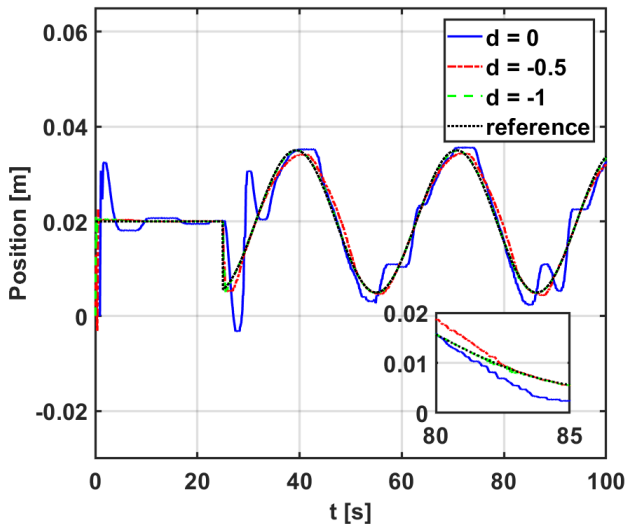
$$\dot{e}_2 = e_3$$

$$\dot{e}_3 = -k_3 \lambda^{-\frac{d}{4+2d}} \left[ [e_3]^{\frac{4}{4+2d}} + k_2^{\frac{4}{4+2d}} \lambda^{-\frac{4d}{(4+d)(4+2d)}} [e_2]^{\frac{4}{4+d}} + k_2^{\frac{4}{4+2d}} k_1^{\frac{4}{4+d}} \lambda^{-\frac{12d}{(4+d)(4+2d)}} e_1 \right]^{\frac{4+3d}{4}} + z + w(t),$$
$$\dot{z} = -k_I \lambda [e_1]^{\frac{4+4d}{4}}.$$

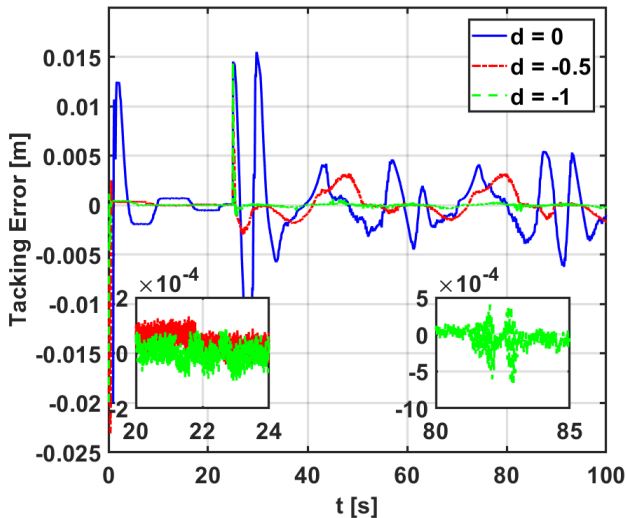
- Homogeneity degree:  $d \in [-1, 0]$

- Euler's integration method of fixed-step, sampling time  $1 \times 10^{-4}[s]$ .
- Gains:  $k_3 = 21$ ,  $k_2 = 7$ ,  $k_1 = 3$ ,  $k_I = 2$
- $d = 0$ : Linear controller.  $\lambda = 100$ .
- $d = -0.5$ . Continuous Nonlinear I-Controller.  $\lambda = 2$
- $d = -1$ : Discontinuous I-controller.  $\lambda = 2$

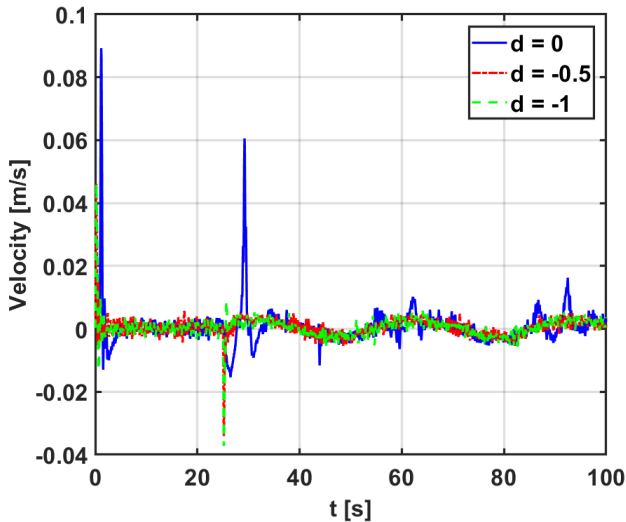
# Experiment 1: Position Tracking



# Experiment 1: Tracking error

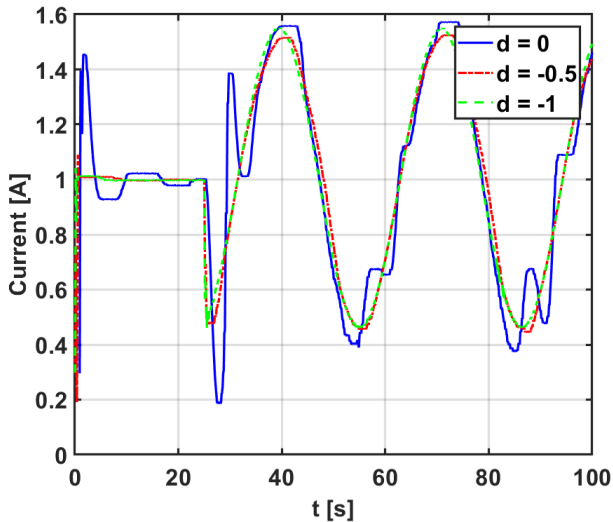


# Experiment 1: Velocity

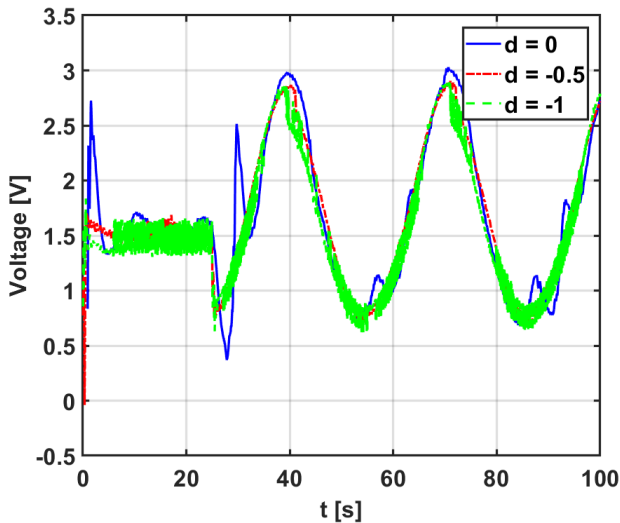




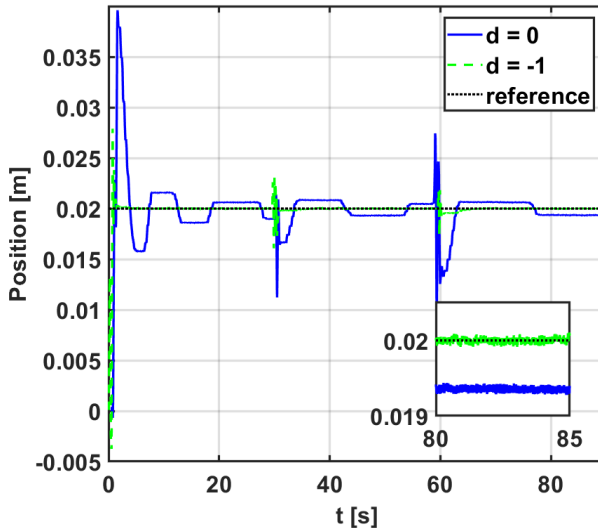
# Experiment 1: Current



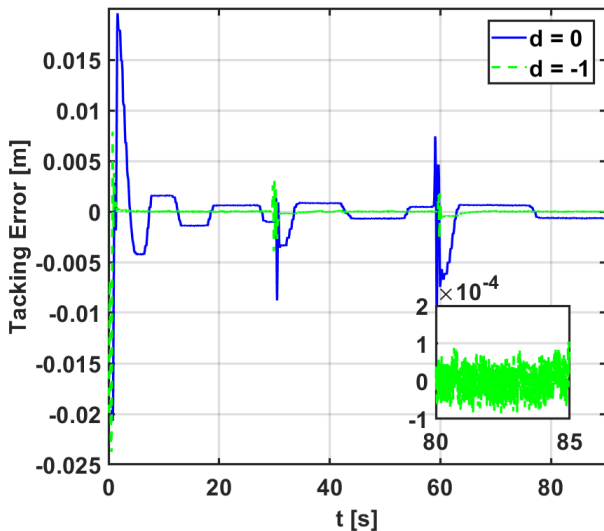
# Experiment 1: Control Signal



## Exp. 2: Position with varying mass

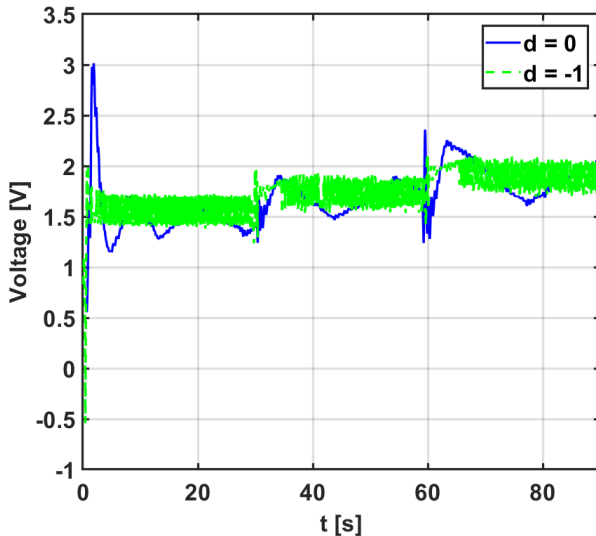


## Experiment 2: Regulation error



1

## Experiment 2: Control Signal



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- Discontinuities seem to be **simple** models for a large class of signals.
- They lead to **simple** solutions for robust control and observation problems.
- Many issues to be studied:
  - Effect of Noise.
  - Implementation: Explicit determination/avoidance of discontinuities.
  - Discretization.
  - Control Design.
- Extensions and uses of Multivalued Observers.
- We can learn from simple problems and systems!

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